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(57) Abstract

The invention relates to a process for producing simultaneously food-grade and fodder-grade phosphoric acid by crystallizing phosphoric acid hemihydrate, $\rm H_3PO_4$ x 0.5 $\rm H_2O$, from a prepurified feed acid, which is purified and crystallized with the help of the following steps,

- a) after the step of froth-flotation of phosphate concentrate, the concentrate is directed to a strongly magnetic separation step in order to decrease the Mg ion amount.
- b) the phosphate concentrate is leached in a mixture of sulfuric acid and phosphoric acid according to the wet process, the precipitated SO₄ and As ions are removed, and a silicon source is added in order to adjust the F/Si molar ratio to < 6.</p>
- c) the phosphoric acid is concentrated, the solids precipitate is removed, and the ${\mathbb F}$ ions are evaporated,
- d) the feed acid obtained from step c, having a concentration of >58% P_2O_5 , solids concentration of <0.05%, Mg ion concentration of <1.5%, SO₄ ion concentration <1%, As ion concentration of <8 ppm and F ion concentration of <0.2%, is crystallized at a steady crystal growth rate of $<10~\mu\text{m/min}$, the temperature difference in the first crystallization being $<17~^{\circ}\text{C}$, and the crystals are washed with the undersaturated mother liquor of the subsequent recrystallization step,
- e) the phosphoric acid crystallized in step d is melted, is diluted to a concentration of $<63\%\ P_2O_5$, seed crystals are added, and crystallization is carried out as in step d, the temperature difference being <8 °C, and the crystals are washed with an undersaturated solution of phosphoric acid, and
- f) optionally the phosphoric acid crystallized in step e is melted, is diluted to a concentration of < 63% P₂O₅, seed crystals are added, and crystallization is carried out as in step d, the temperature difference being < 6 °C, and the crystals are washed with an undersaturated washing solution prepared from product crystals.</p>